



# HYDR<sup>o</sup>met

## Heap leaching of copper ores – opportunity through science

Jochen Petersen



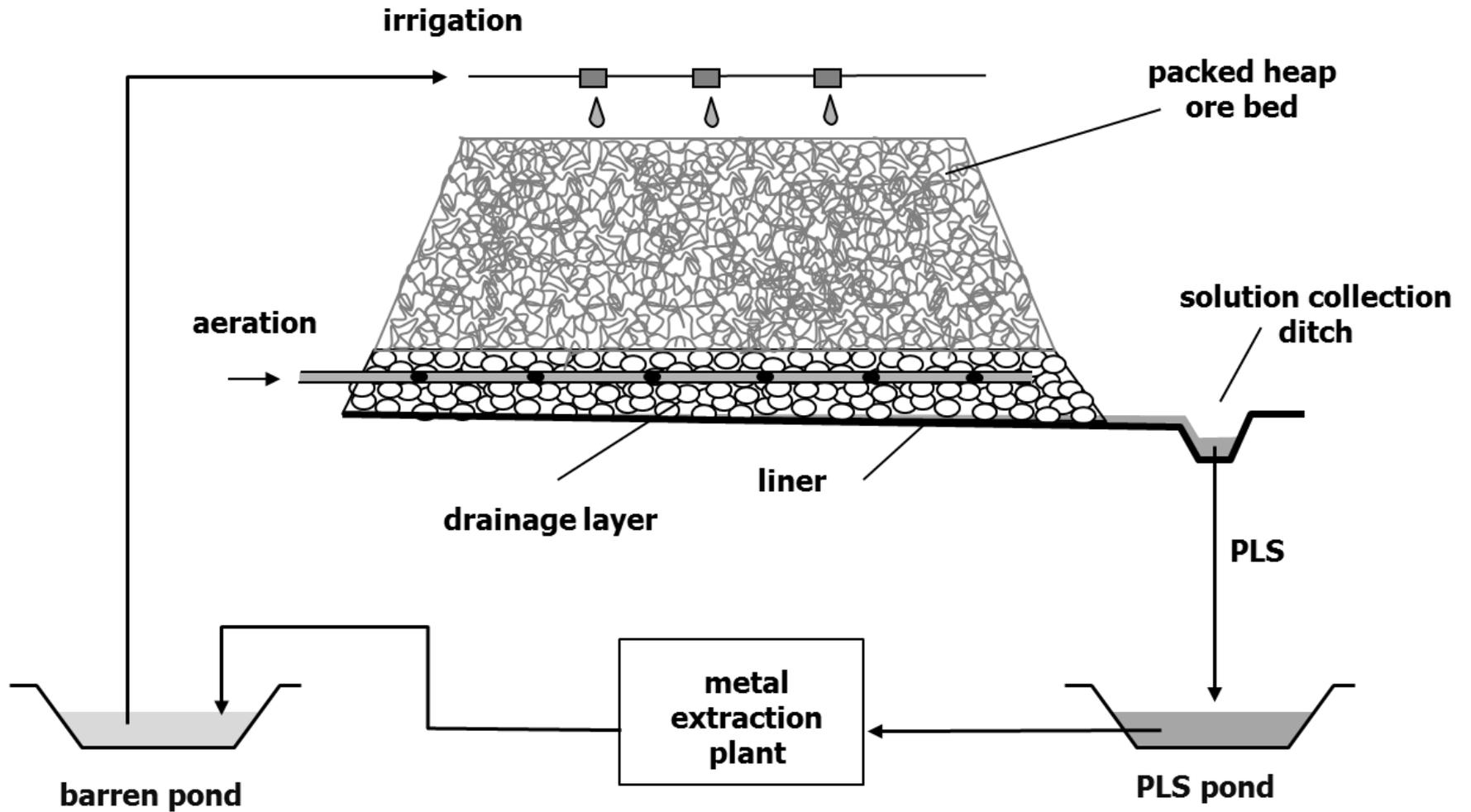


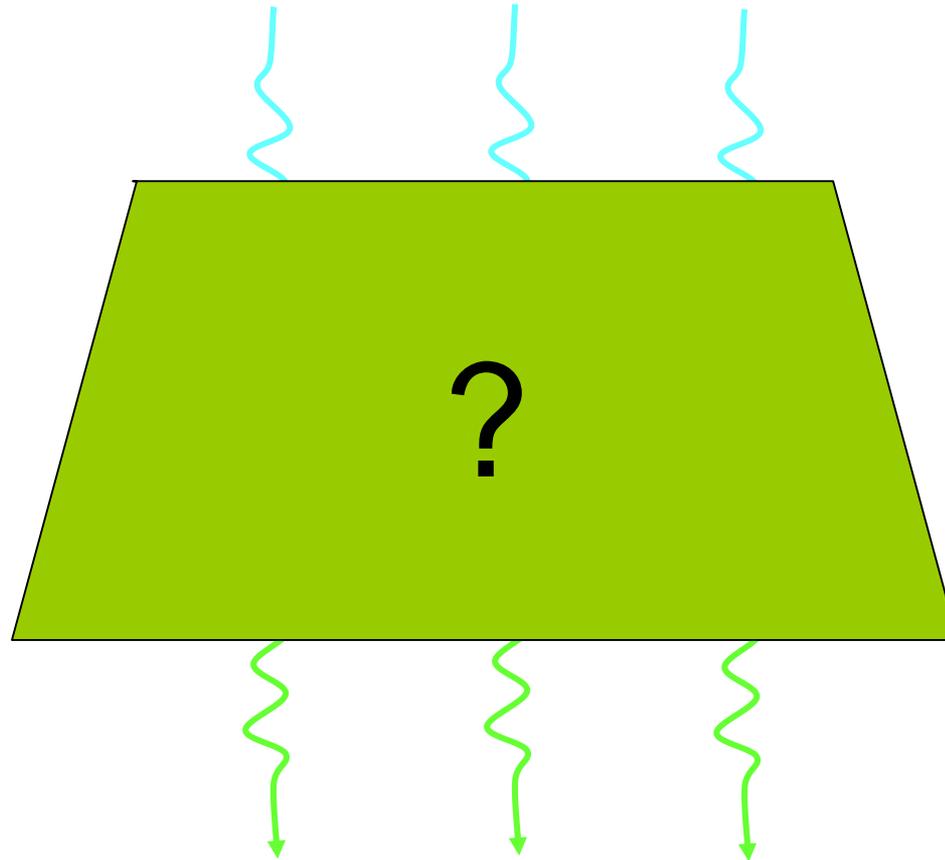
# A typical heap leach operation

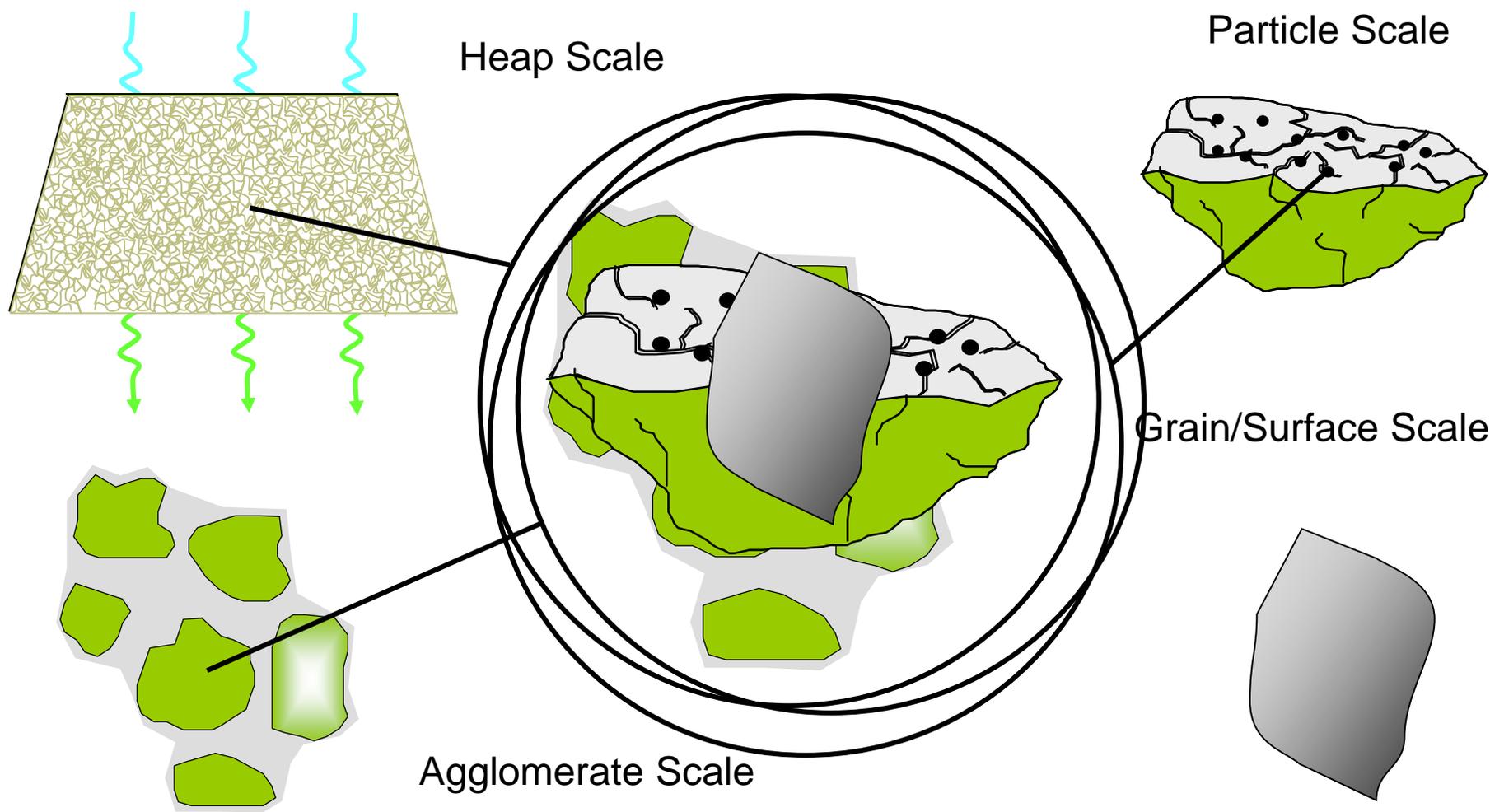




# Heap leach process







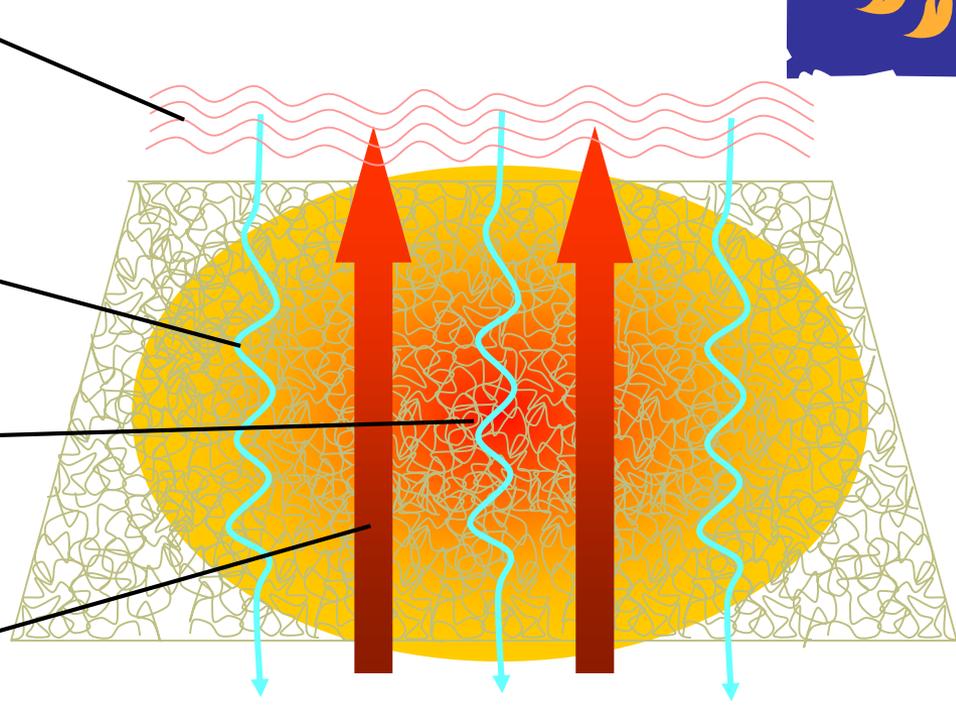


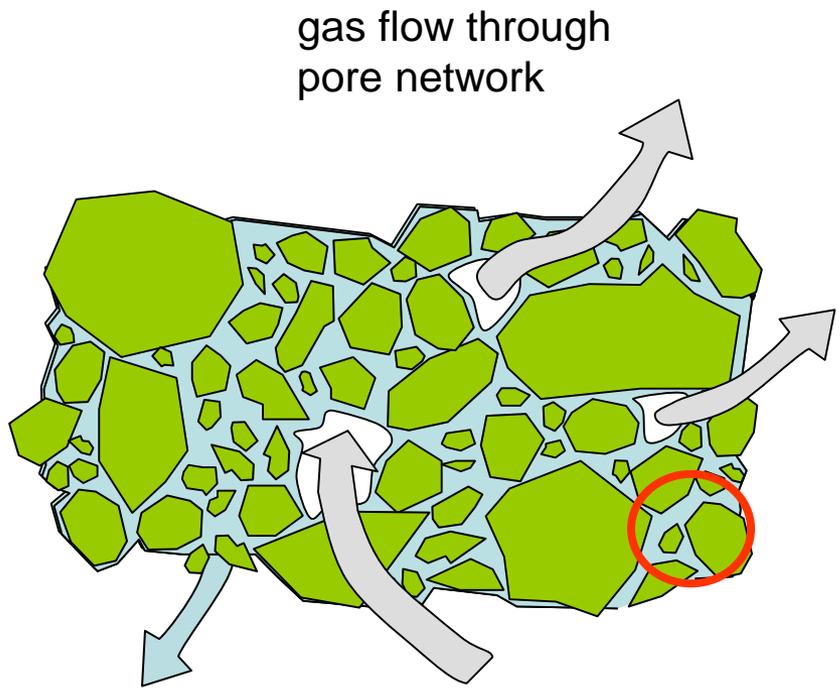
Surface evaporation and radiation

Solution flow downwards

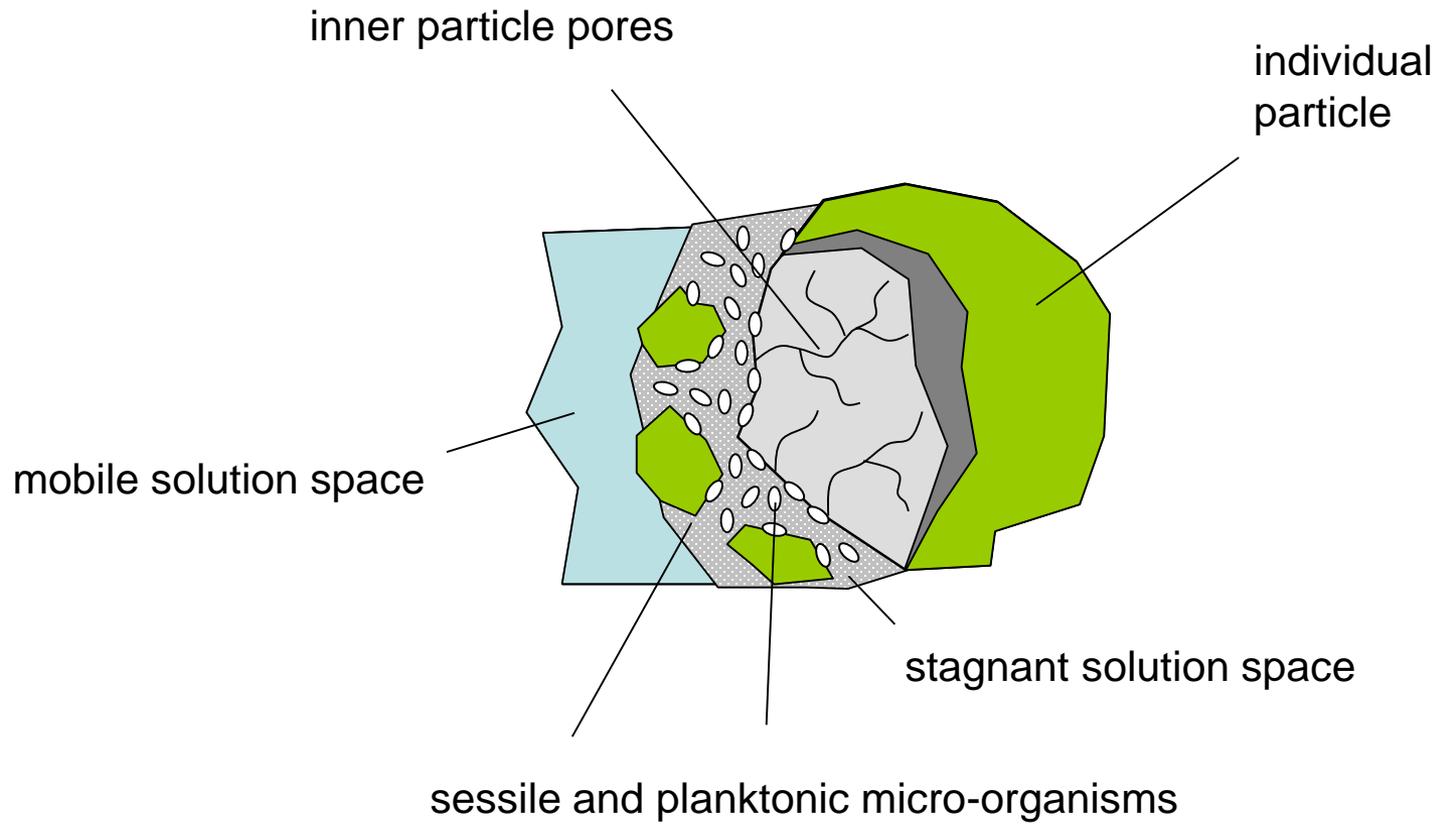
Heat generation through reaction

Gas (humid air) transport up



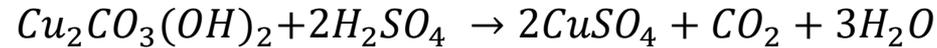


Solution 'seeps' along preferential channels  
on air-liquid contact surfaces





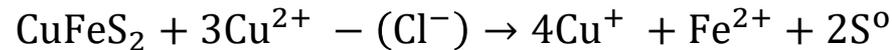
Acid leaching of malachite



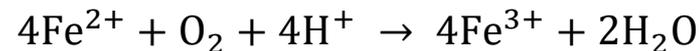
Ferric leaching of covellite



Chloride facilitate leaching of chalcopyrite



Ferrous re-oxidation (biologically accelerated)



Cuprous re-oxidation (rapid in chloride solution)

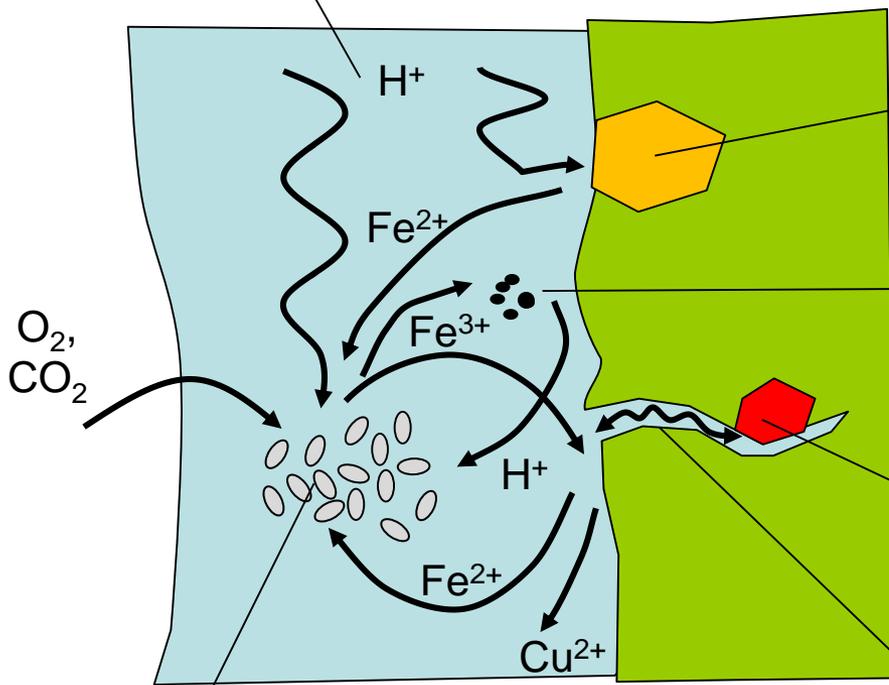


Sulfur oxidation (chemically or biologically facilitated)

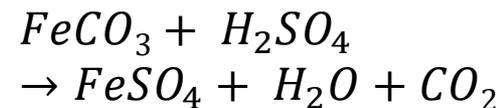




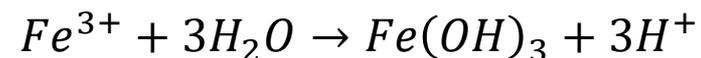
acid migration or flow through liquid film



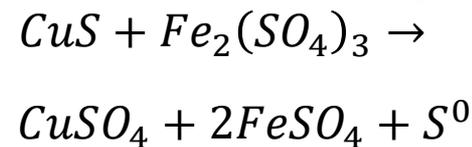
reaction with gangue grains



$Fe(OH)_3$  precipitation



reaction with mineral grains



gas phase

solution phase

solid phase

re-oxidation of ferrous (biological or direct)

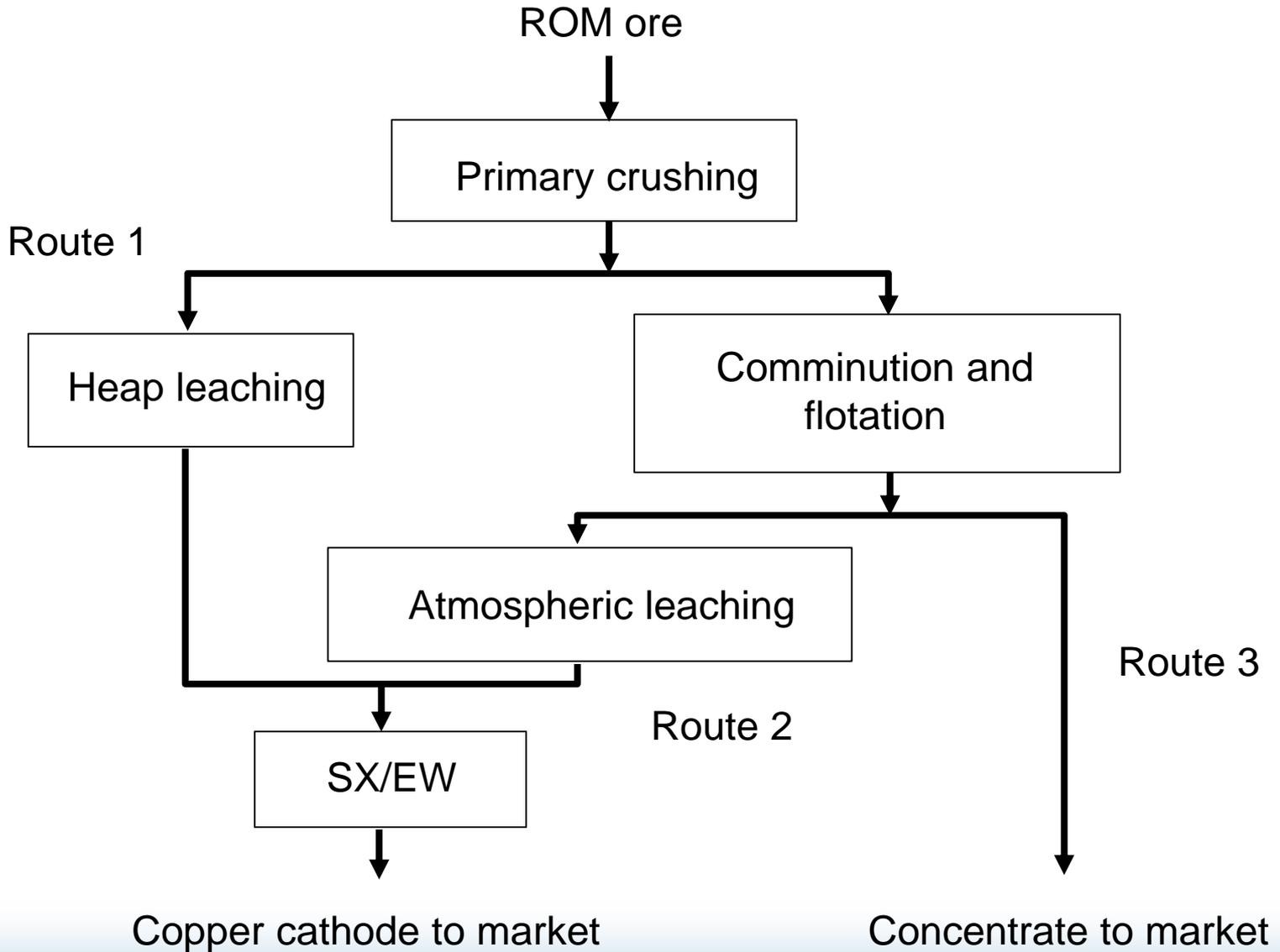
diffusion through micro-pores

## Is heap leaching a competitive technology?

- Slow process, residence time of months to years
- Poorer extraction (70-80%)
- Large physical footprint
- Long-term environmental burden uncertain

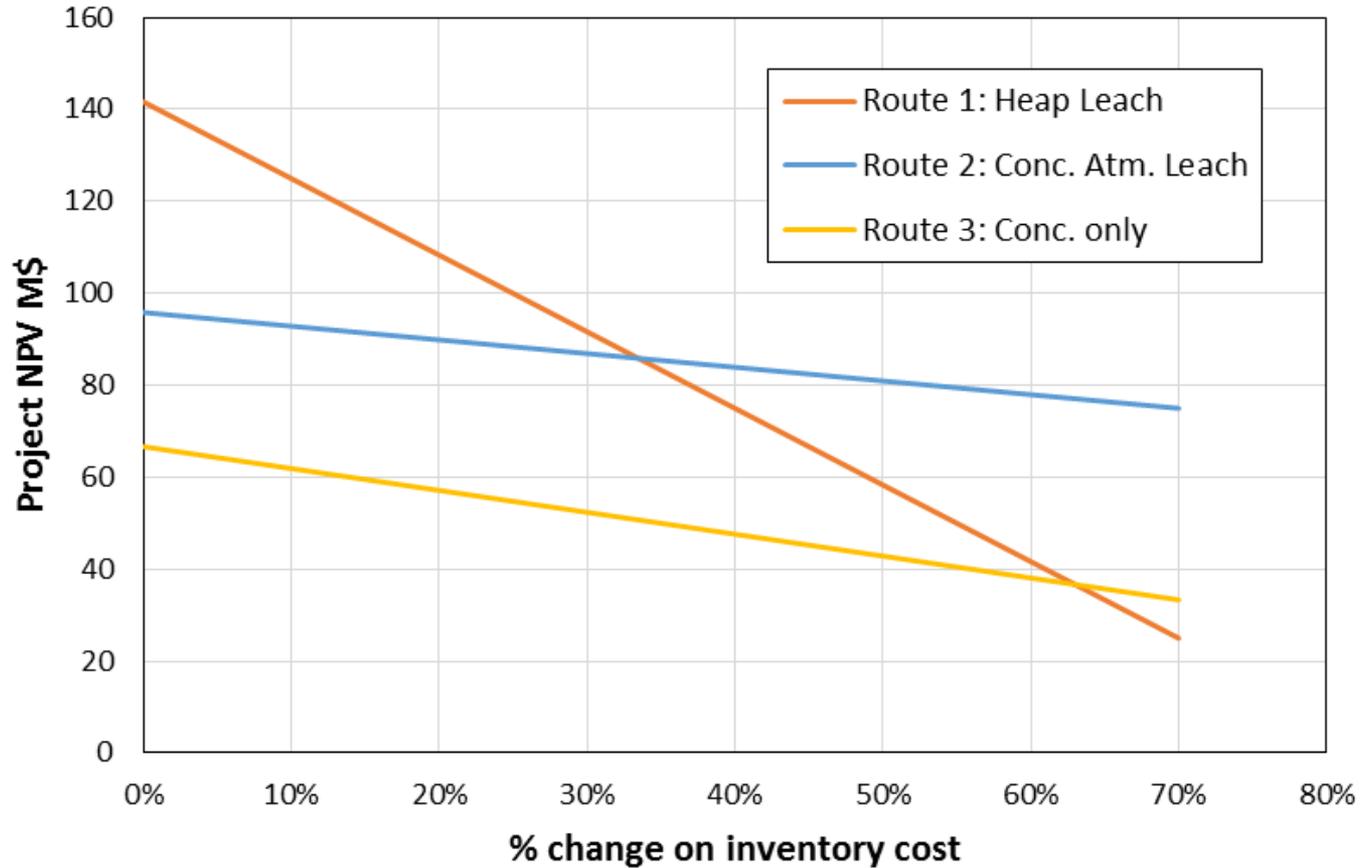
BUT

- Low energy requirements (crushing instead of milling)
- Simple, low-cost technology, can operate at remote sites
- Spent heaps comparable to tailings dams from minerals processing





### Effect on inventory on NPV



In heaps, inventory cost is directly linked to tons of ore under leach/ leach time

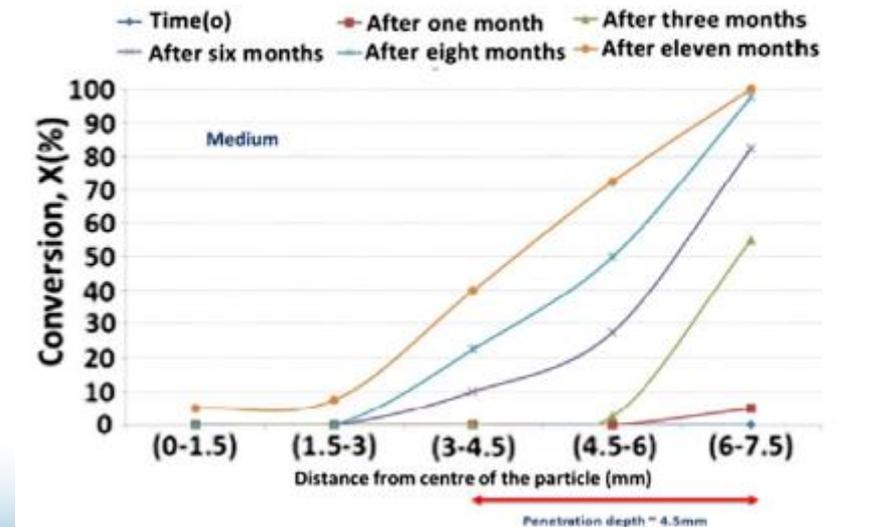
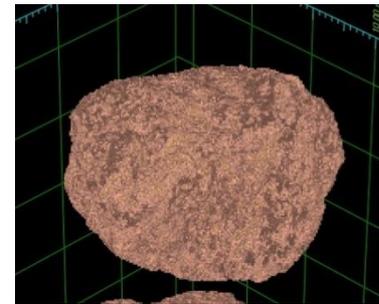
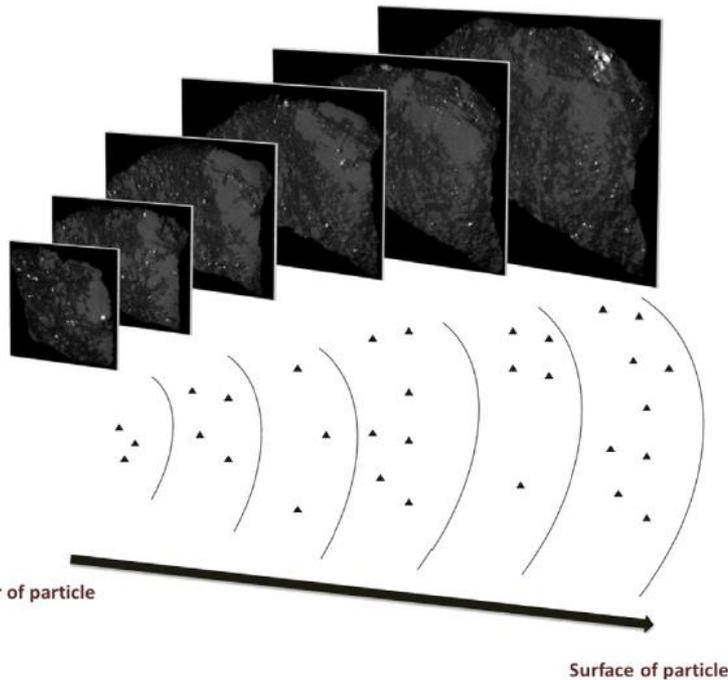


## Why is heap leaching often so slow?

- Slow reaction kinetics at low temperatures
- Unliberated minerals in large particles
- Low aeration rates and poor gas-liquid mass transfer
- Solution channelling and stagnant zones
- re-adsorption of Cu onto precipitated Fe phases

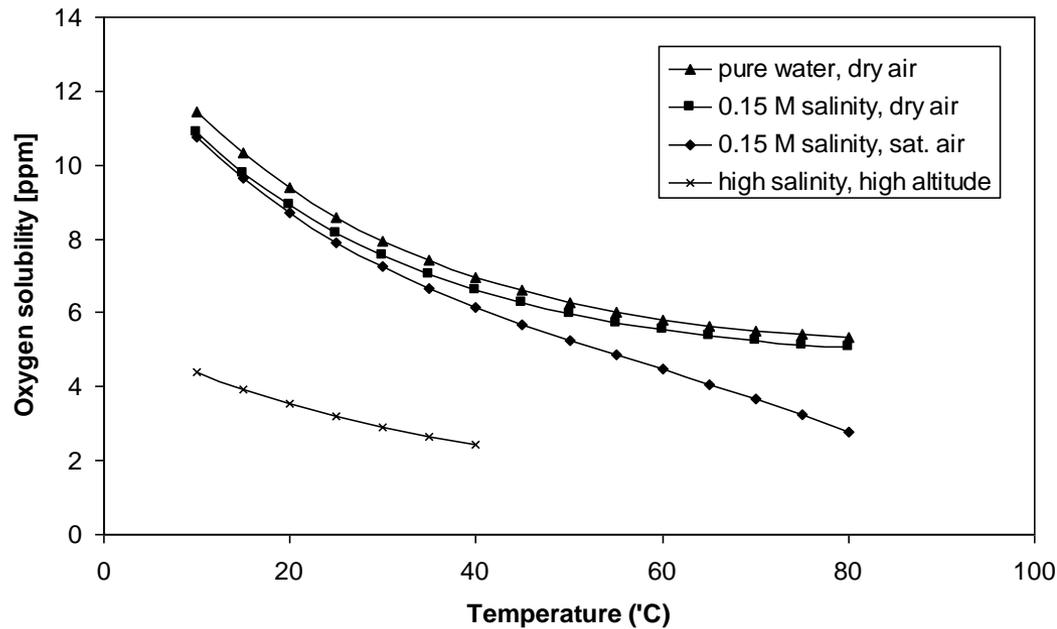
## Mineral extraction from large particles

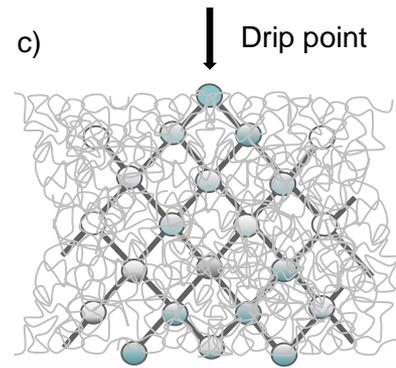
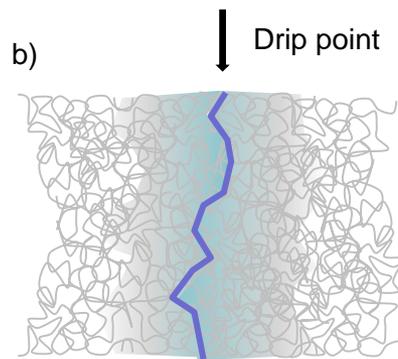
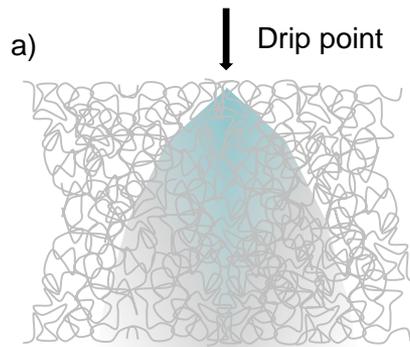
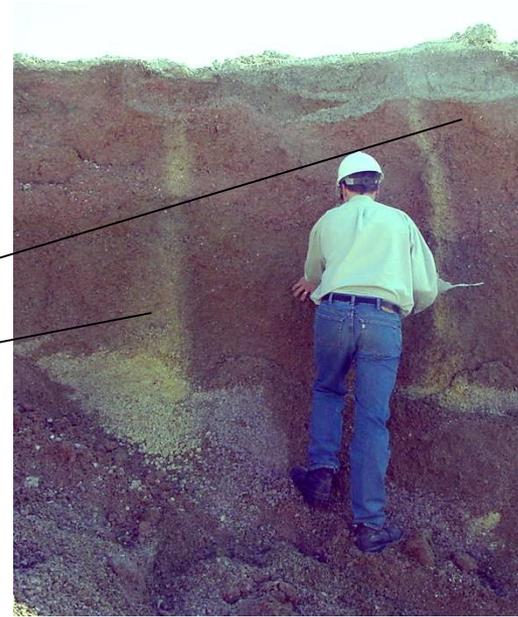
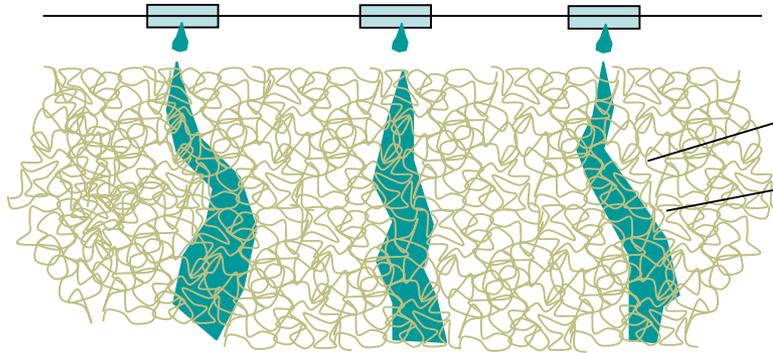
- X-ray tomography shows shrinking shell and unreacted core

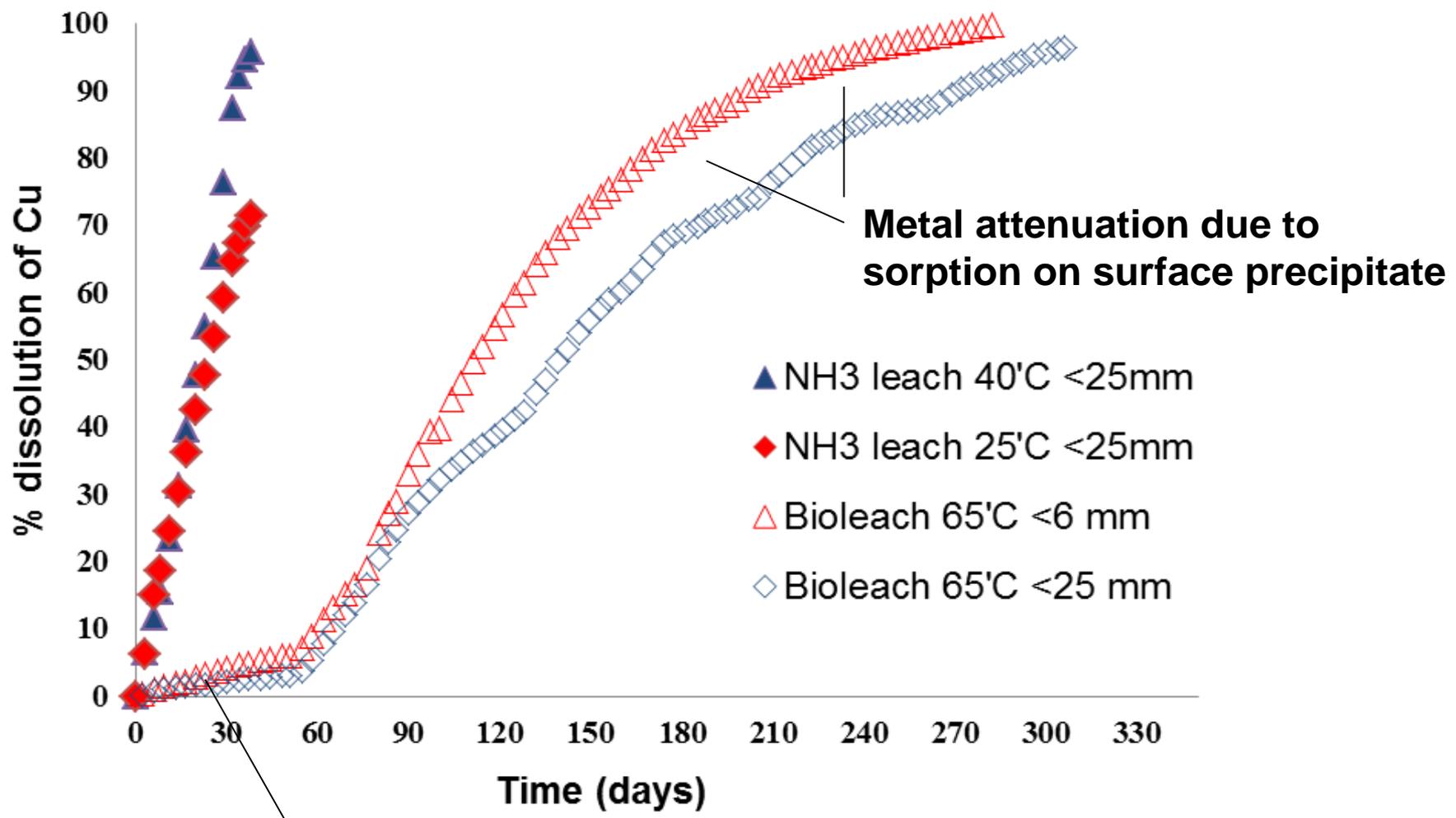


## Gas-liquid mass transfer

- rate limited by low  $O_2$  solubility and interfacial area
- $O_2$  solubility limited by temperature, solution salinity and air pressure



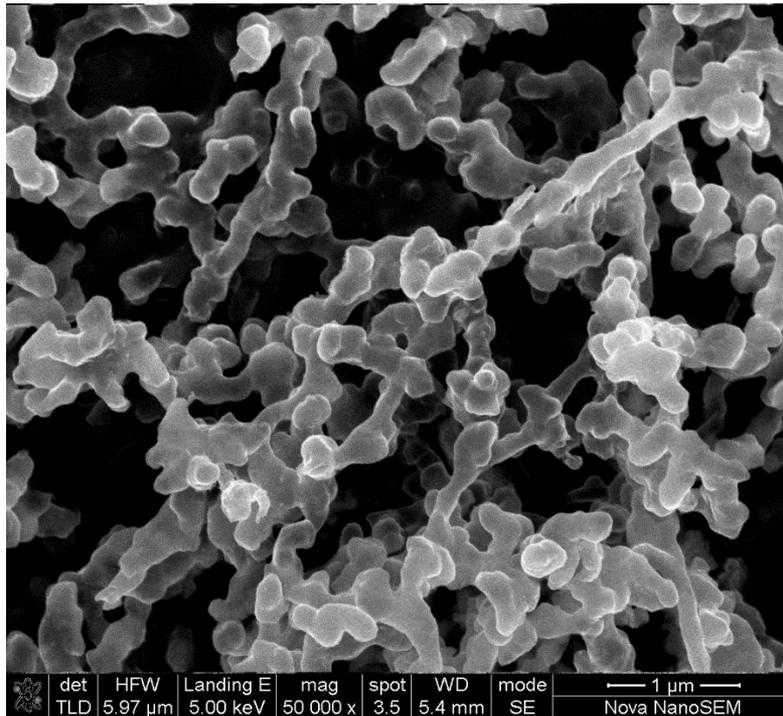




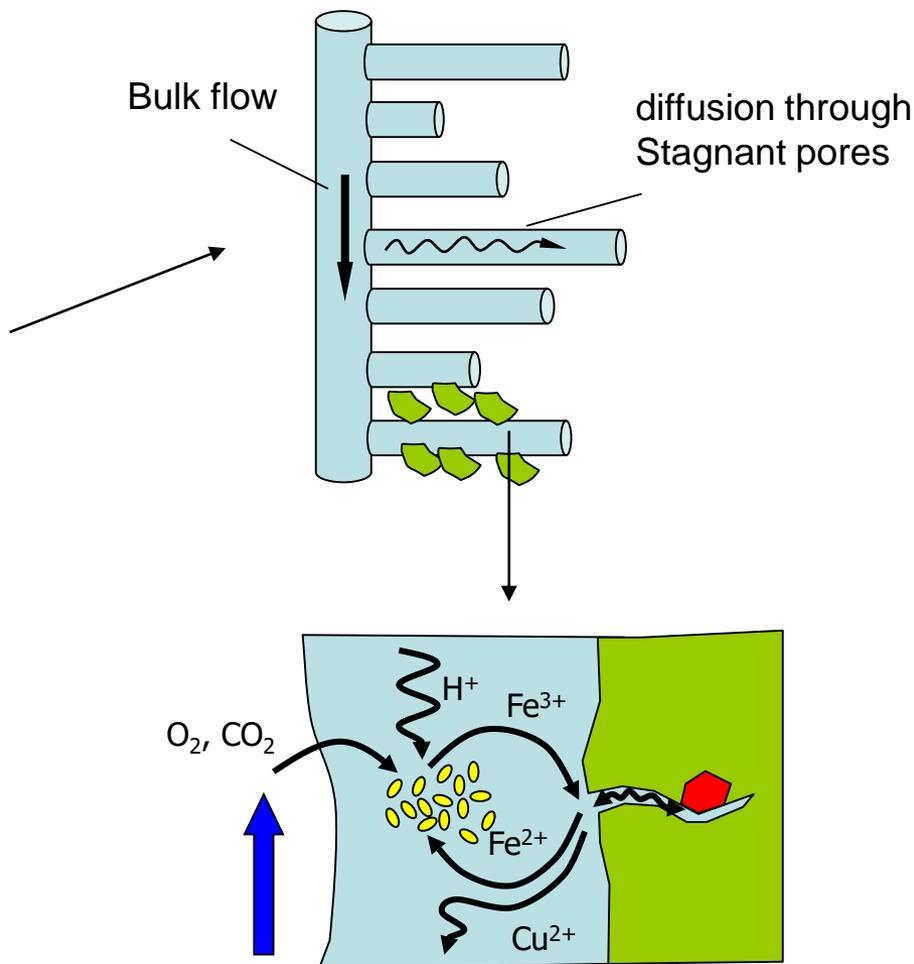
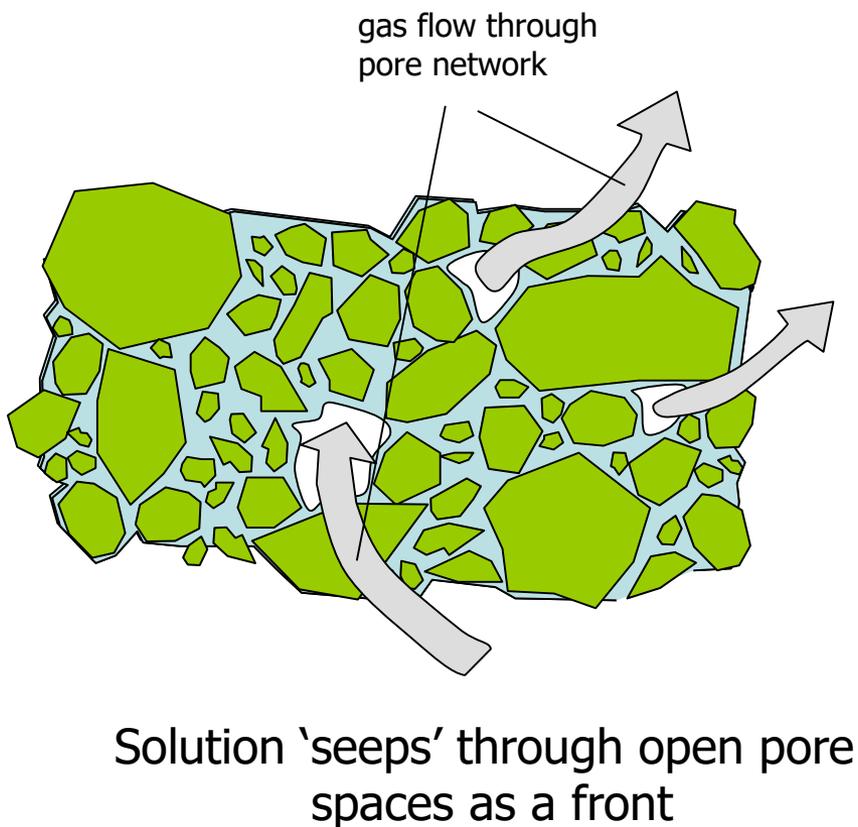
- Progressive 'cementation' of heap ore by Fe-precipitates



- Nano SEM studies of freshly precipitated Fe-OH
- Network structure of precipitate offers large surface for metal sorption and inhibits solution flow

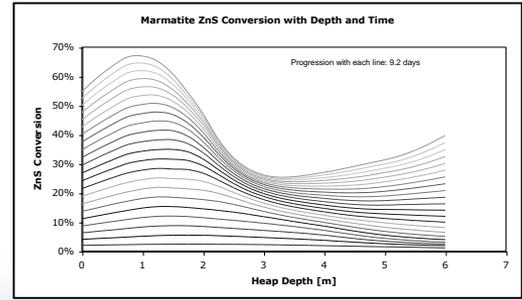
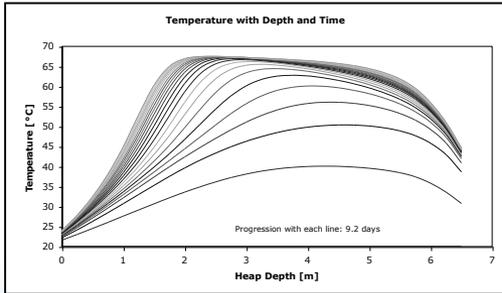
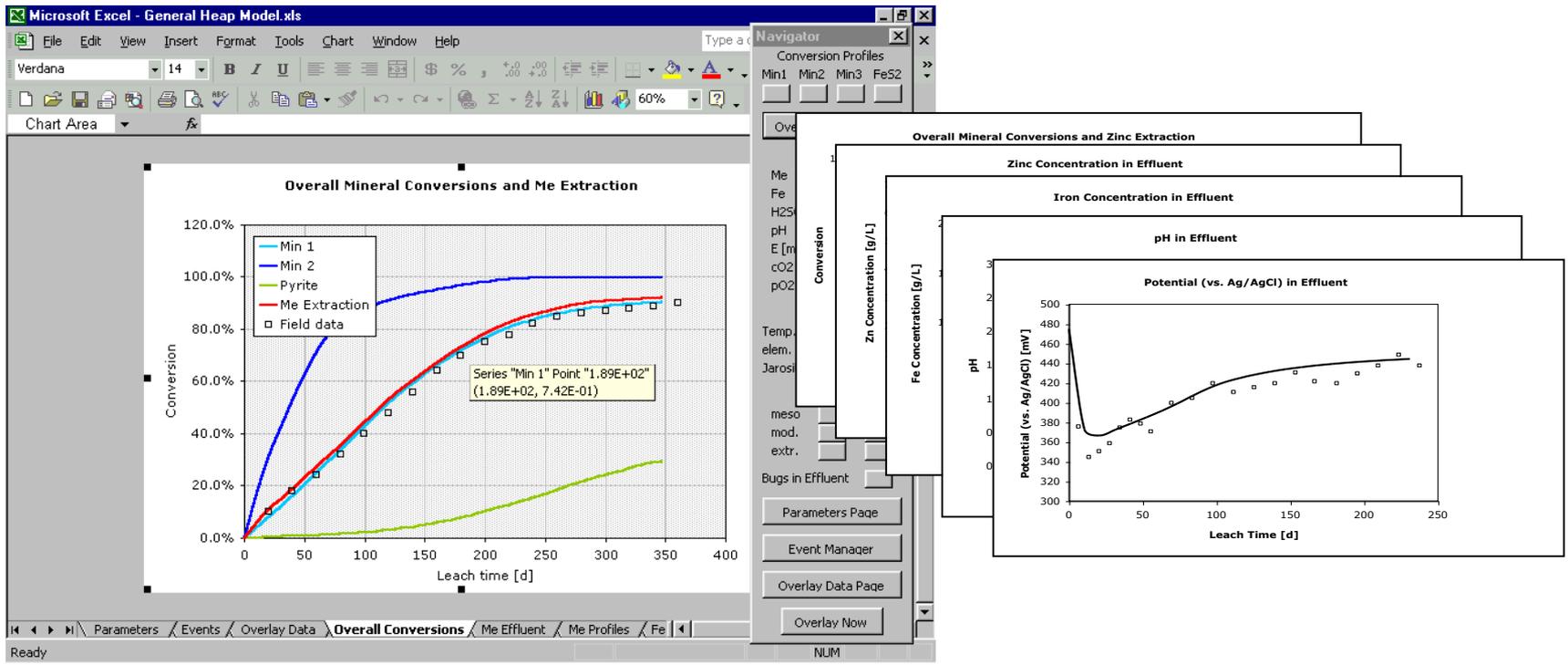


## Transport-reaction modelling





## HeapSim Model





- Complex distributions of reagent and heat distribution throughout heaps determines local rates of leaching;
- Ambient conditions have significant impact on oxidative heap leaching;
- Optimal heap design varies strongly with ore characteristics;
- There are 'speed limits' to the maximum rate of leaching:
  - Supply rate of acid (rare)
  - Reagent distribution through stagnant (diffusion) zones
  - Mineral liberation in large particles
  - Supply rate of oxidant (air) – gas liquid mass-transfer
  - Formation of adsorption buffers



- Heap leaching is a technically simple process, but of immense physical complexity at all scales.
- The interplay of these complexities is difficult to grasp, yet understanding them offers opportunities to conduct the process efficiently.
- Economic analysis indicates if heaps can be made to operate reliably at their optimum, they would be a serious technology of choice.
- Heaps do have a future!

# Thank You



The National Research Foundation (NRF) of South Africa is acknowledged for funding this research through their Incentive Funding for Rated Researcher programme.

